

Process Systems Engineering for the sugar industry: concept and applications

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Audubon
Sugar
Institute

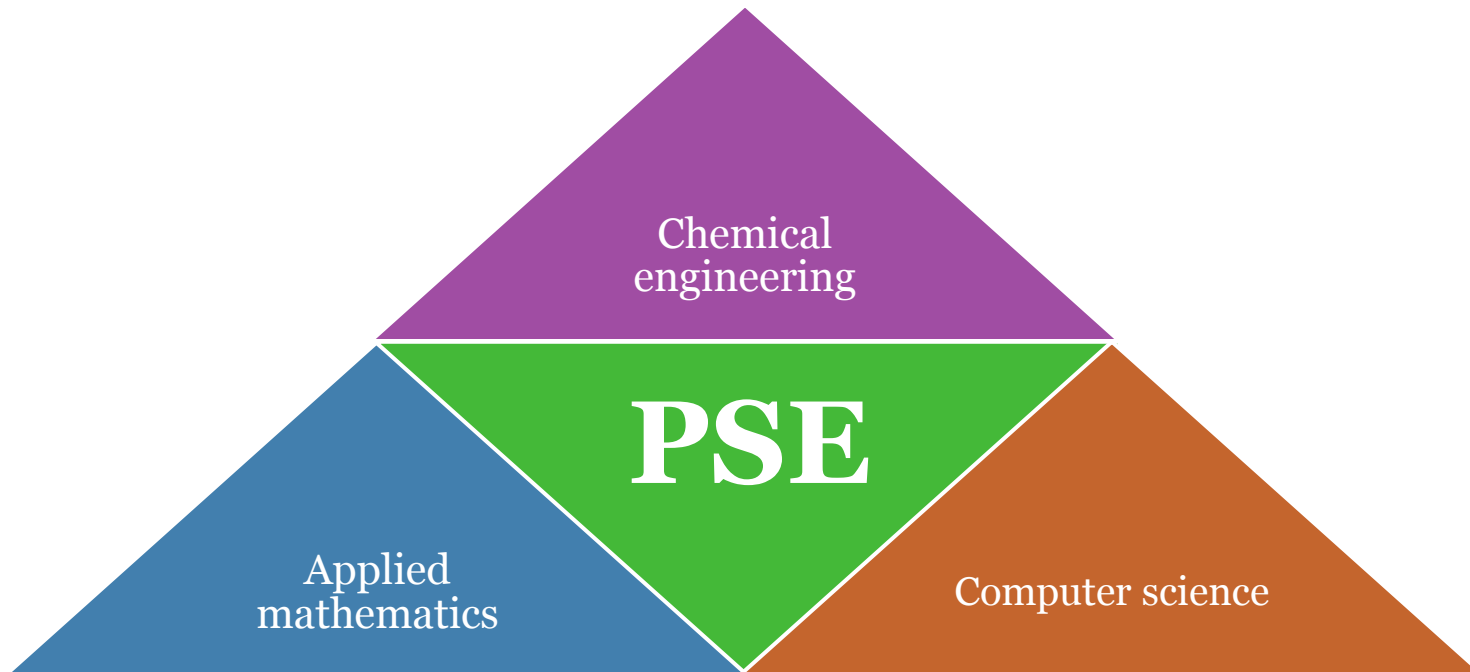


Overview

- What is Process Systems Engineering (PSE)
 - Generalities
 - Process models
- PSE's Activities
 - Simulation
 - Process control
 - Process optimization
 - Planning and scheduling
- Conclusion

Process Systems Engineering (PSE)

Planning, design, operation and control of physical, chemical and biological processing operations



Process Systems Engineering

Mathematical modeling of the individual components in a system and **their interactions**, is the essential element of all modern PSE activities

Process model
(mathematical equations)

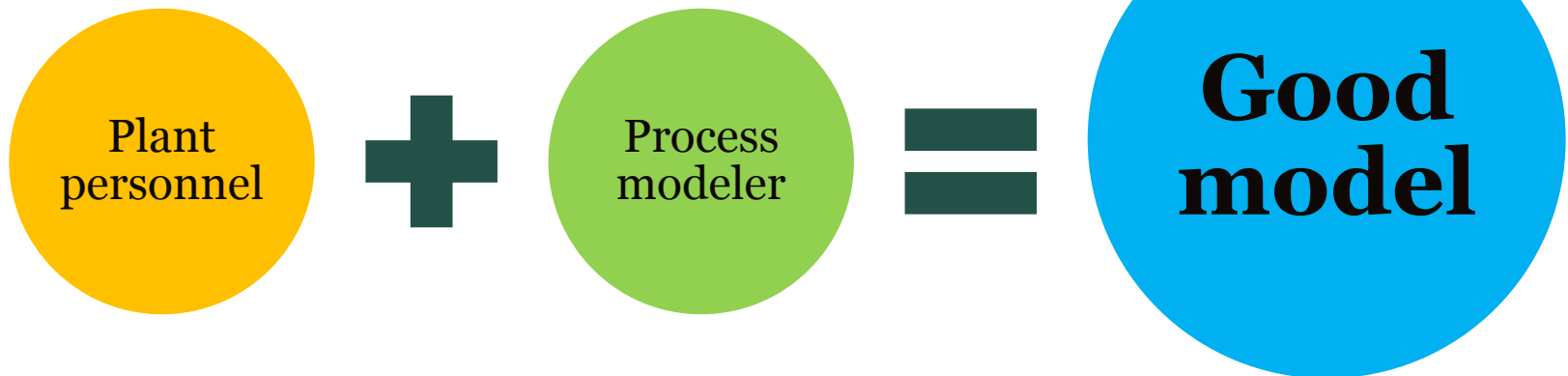
Represent the
behavior of the
process

Are not 100%
accurate

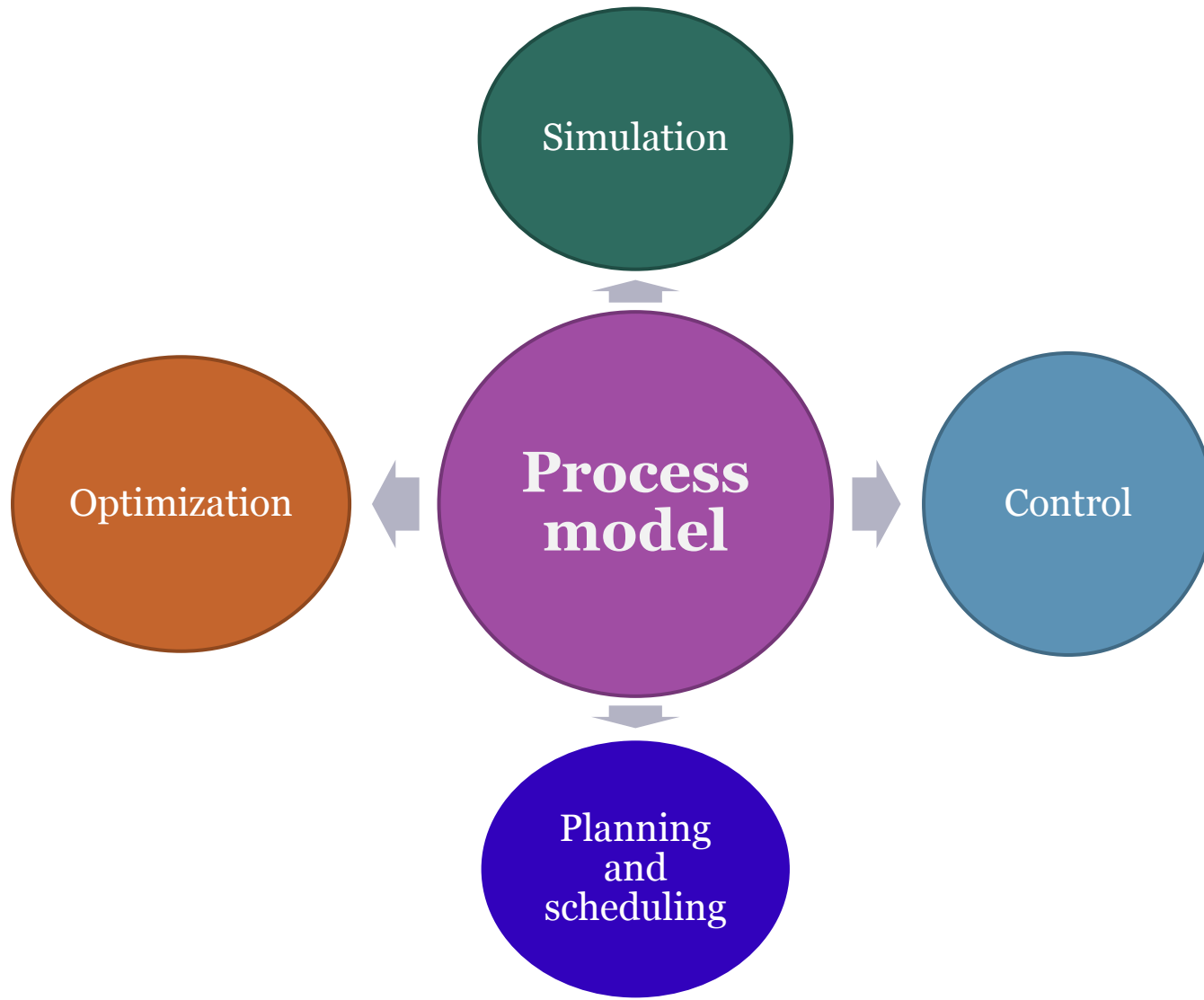
Have a specific
region of
applicability

Process Systems Engineering

A good model has the **required accuracy** and **gives answer** to the problem stated by the purpose of modeling



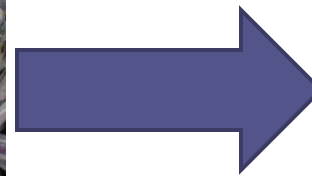
PSE's Activities



Simulation

Use of a process model to obtain a response given certain input values

Cane
Ton/day
Pol
Fiber
...



Solution to model equations



Filter cake
Ton/day
Pol
...

Applications: operator training, factory balances, new equipment installation, evaluating changes in operative conditions, ...

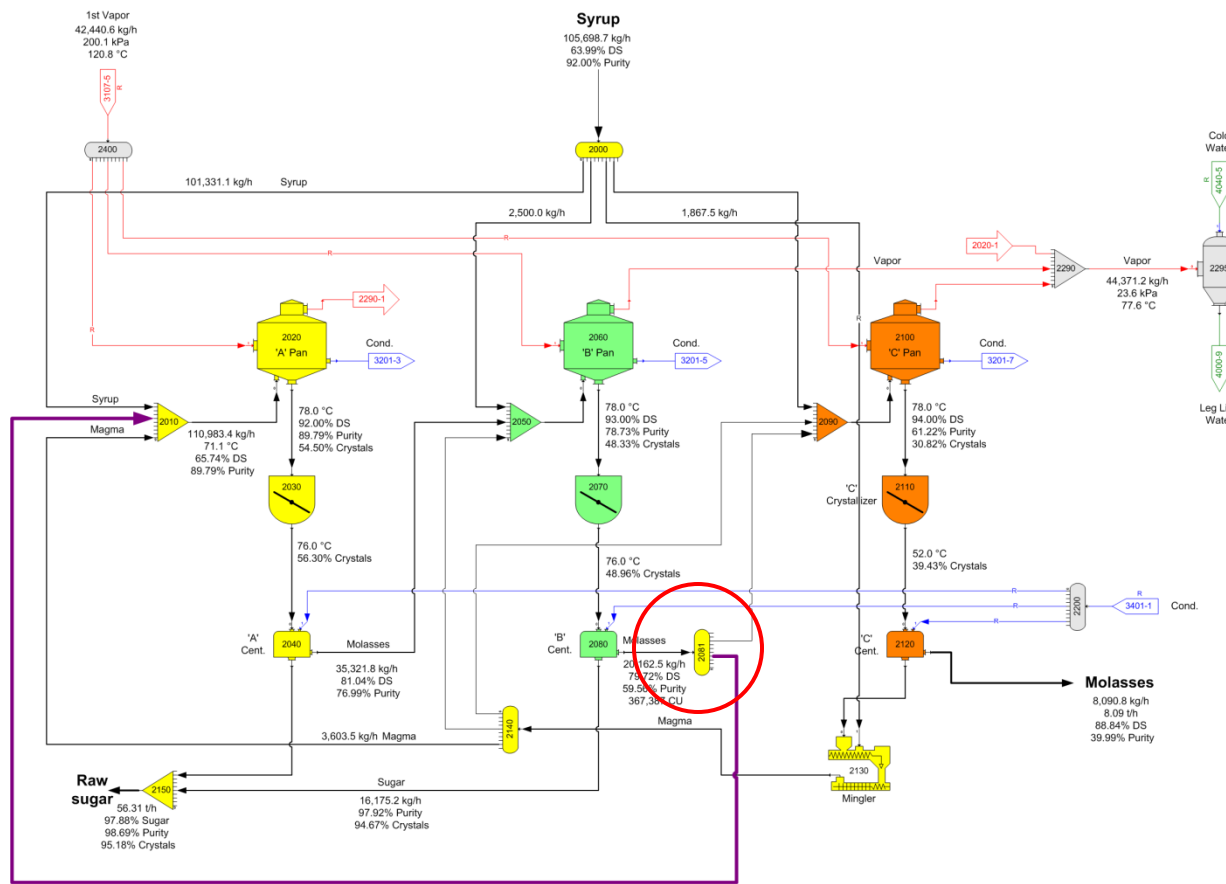
Simulation can reduce costs and risks from experimentation

Simulation Example

- Changes in process conditions in sugar boiling operation
 - Three boiling scheme
 - Syrup purity changes from 85% to 92%
 - What is the change in final molasses purity?
 - How does final molasses purity changes when recycling B molasses into A pans to reduce syrup purity?
 - Model created in SugarsTM

Simulation Example

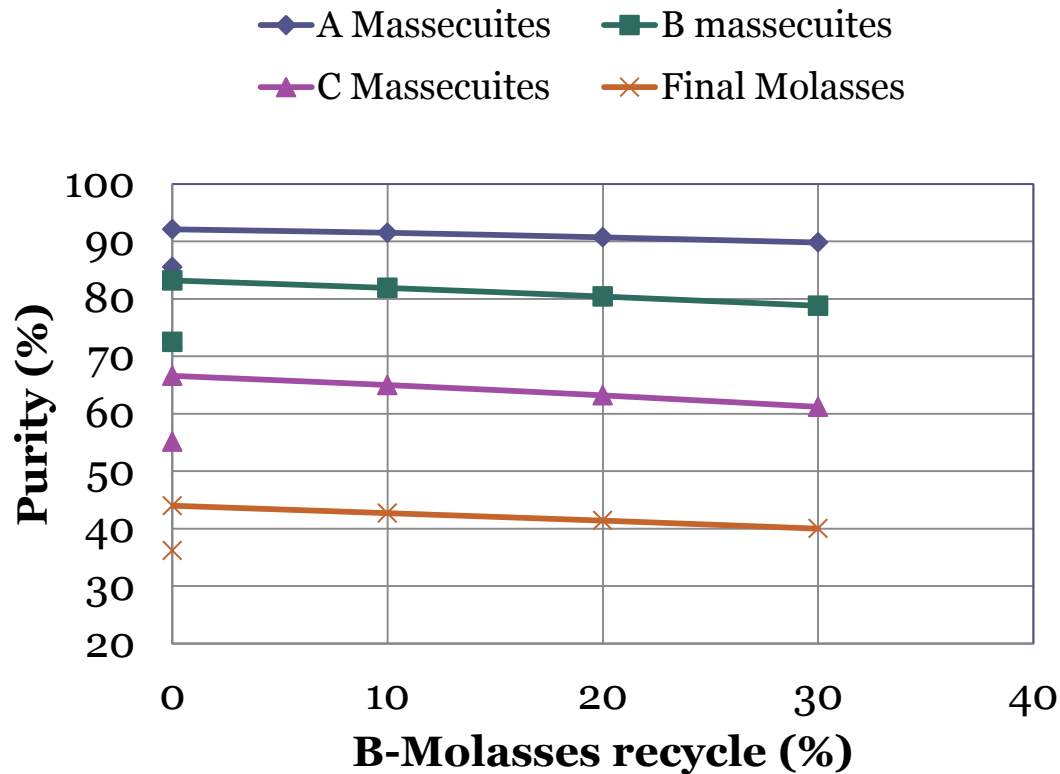
Three boiling scheme with B molasses recycle into A pans in Sugars™



B molasses recycle

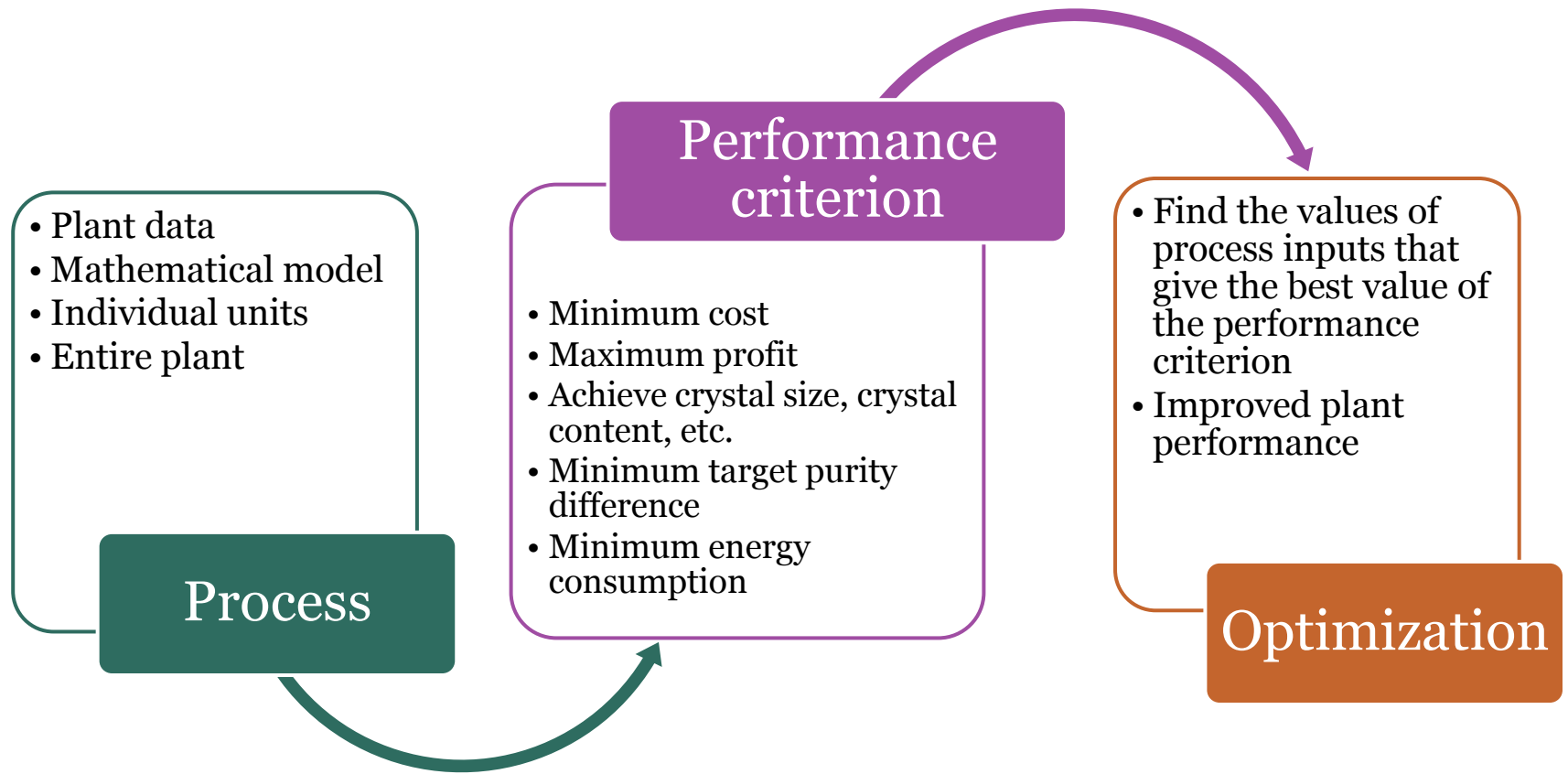
Simulation Example

- Effect of B-molasses recycle on purity of massecuites and final molasses



Final molasses
purity decreases
1.3% per each 10%
of B molasses
recycled

Process Optimization



Optimization Example for a vacuum pan¹

- Performance measures in crystallization are conflicting objectives
 - Coefficient of variation (CV)
 - Average crystal size (MA)
 - Crystal content (Wc)
- Objective of optimization
 - Define the optimal profiles of feeding rate of liquor/syrup and steam supply rate, to meet performance measures
 - Desired values
 - MA between 0.55 and 0.6 mm
 - CV less than 30%
 - Wc greater than 50% at the end of the strike
- Results
 - Final values of MA, CV and Wc fall within the desired values (CV=28.2 %, Wc=57%, MA =0.6 mm)
 - Smooth behavior of MA and CV

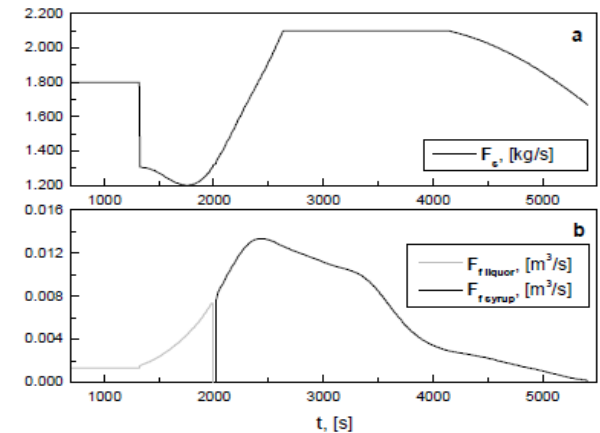


Fig.4. Optimised steam supply (a) and feeding rate (b) profiles, and the optimal switching time.

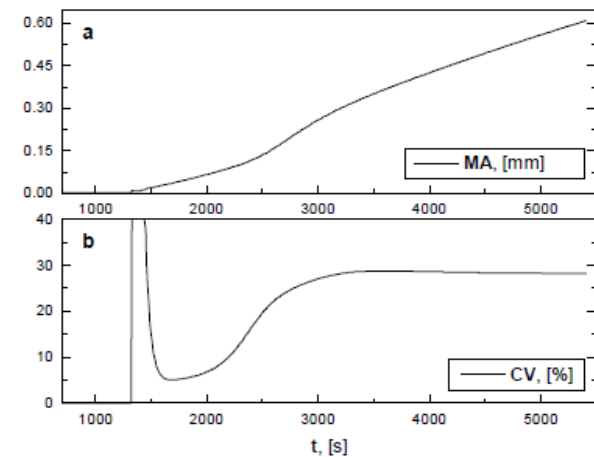


Fig. 6. Average (in mass) crystal size MA (a) and coefficient of variation CV (b) resulting from the optimised control strategy.

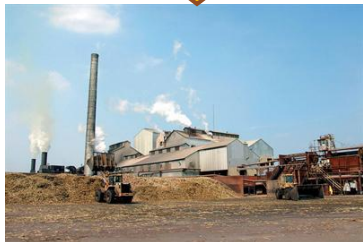
Process Control

The objective of the control system is to keep the process conditions at the desired value in the presence of disturbances or changes in set point

pH control in clarification

Disturbances

Cane variety and quality



Variable pH

Raw juice



Process



Clarifiers

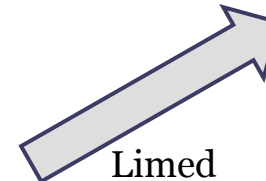


Lime

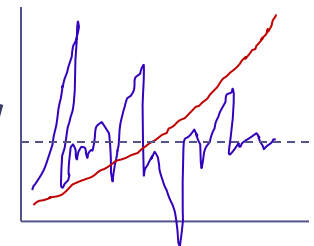
Inputs

Process variables

Poor control



Limed juice



pH of limed juice

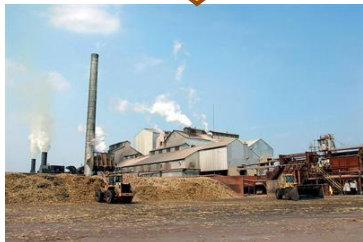
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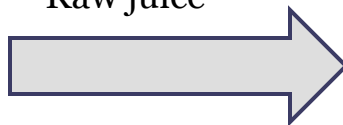
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Process

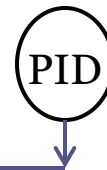
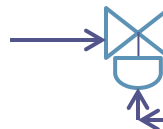


Clarifiers



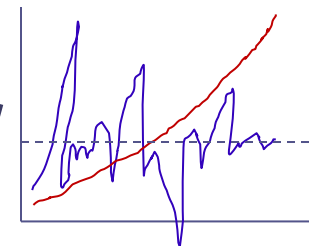
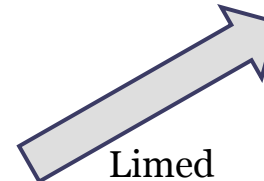
Lime

Inputs

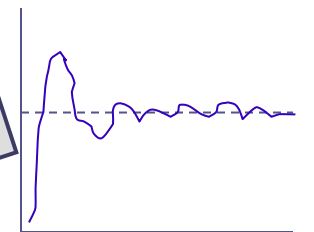
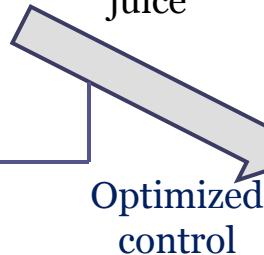


Process variables

Poor control



Limed juice

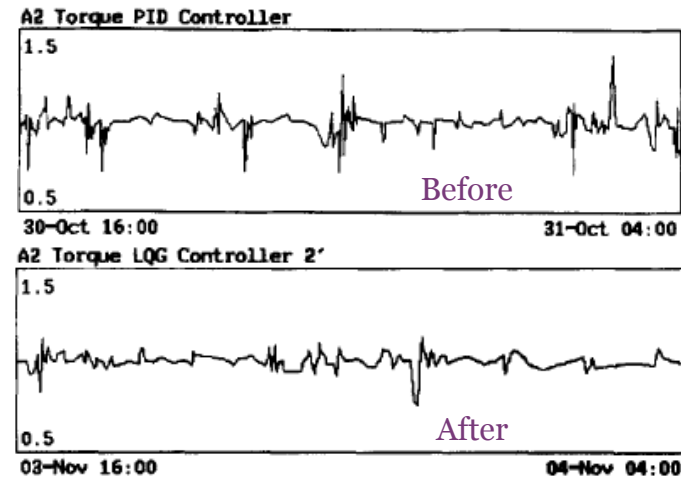


pH of limed juice

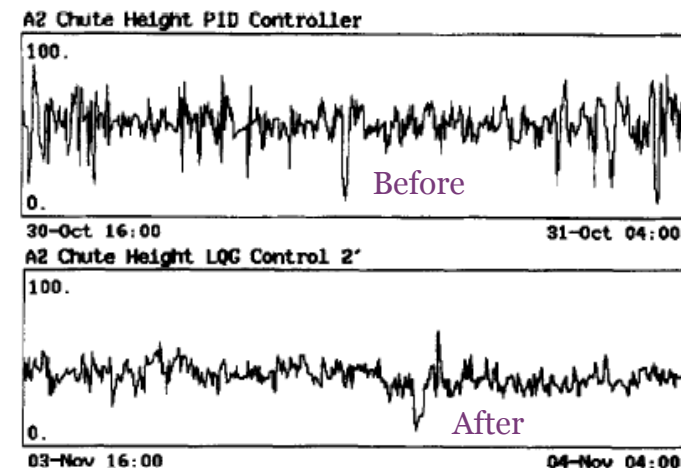
Control Example for a crusher mill²

- High feedstock variation (growers, regions, varieties, etc.) in short periods of time
- Conventional PID is enough to cope with feedstock variations but it could be improved.
- Objective of control
 - Improve torque control maintaining chute height at acceptable levels using advanced process control
- Plant data
 - Cane feed rate, drive torques, chute levels, roll speeds
- Results
 - Advanced control improved results over the conventional PID
 - Torque standard deviation reduced by 40 %
 - Chute height standard deviation reduced by 38 %

Torque log



Chute Height Log



Planning and Scheduling

Corporate Operations Planning

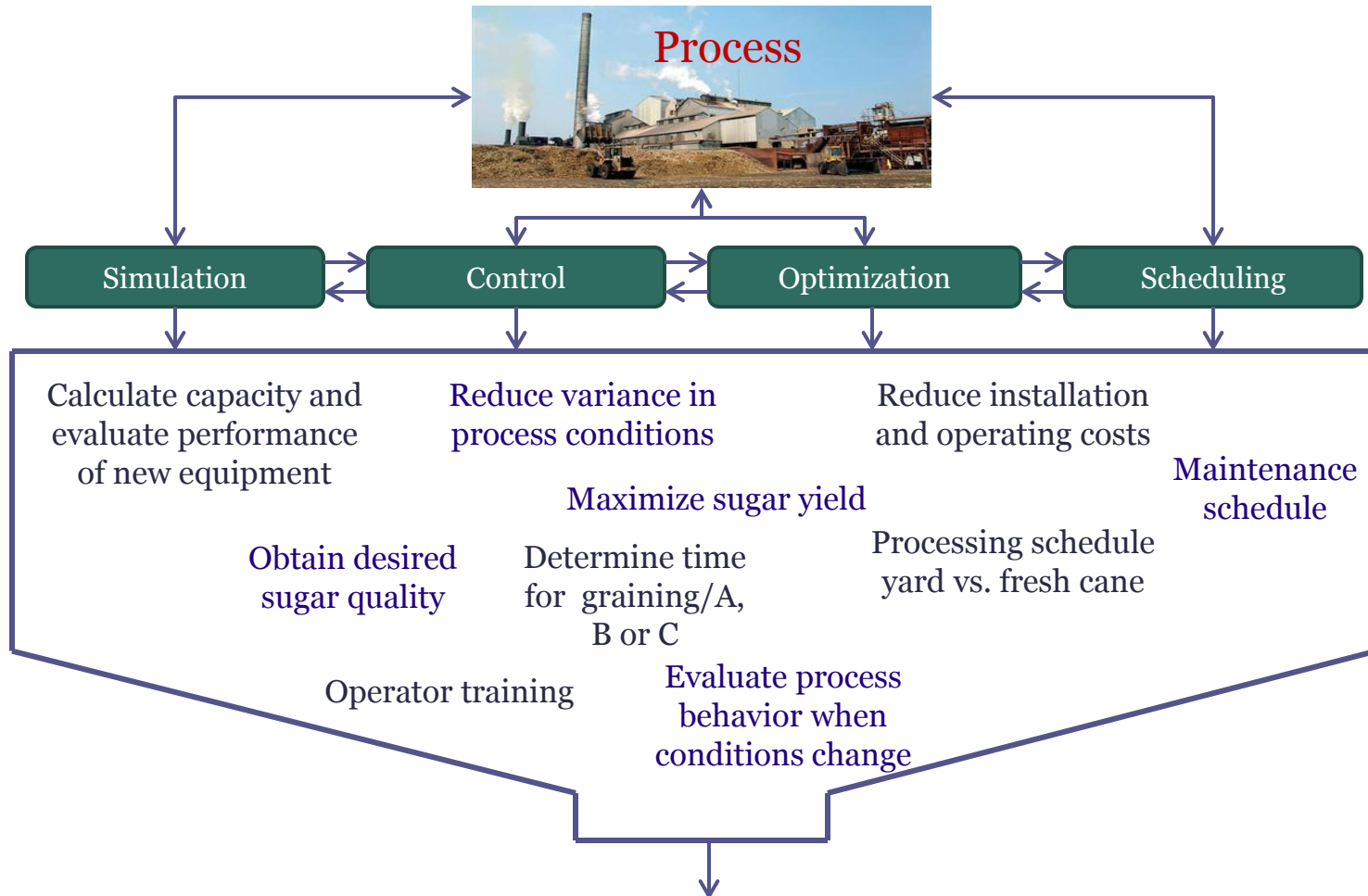
- Optimize materials and product movements (supply chain)
 - Cane harvesting and delivery schedule

Plant Operations Scheduling

- Determine length of runs
 - Batch pans
- Determine sequence of operations
 - Evaporator maintenance schedule



Conclusion



IMPROVED PERFORMANCE = MORE SUGAR = MORE MONEY

Thanks!

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